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(54) Title: CURTAIN COATING PROCESS USING A HIGH SOLIDS CONTENT COMPOSITION, AND COATED PRODUCT

(57) Abstract: The invention relates to a curtain coating process for coating substrates with a stable curtain and a uniform coating at low flow rates wherein a free-falling curtain of an aqueous composition comprising a high solids content is coated onto the moving substrate at a flow rate per unit die length value (Q) equal to or inferior to $10^{-4} \text{ m}^3 /(\text{s.m})$, the said high solids content composition comprising a polymeric rheology modifier and a non-ionic surfactant. The invention relates in particular to a curtain coating process for coating fibrous substrates such as paper or board. The invention also relates to a coated product.

CURTAIN COATING PROCESS USING A HIGH SOLIDS CONTENT COMPOSITION, AND COATED PRODUCT

Field of Invention

5 The invention relates to a curtain coating process using a high solids content composition for coating a substrate web, and to a coated product.

Background of the Invention

In the manufacture of printing paper, pigmented coating compositions are applied
10 by, for example, blade, bar, air-knife or reverse-roll type coating methods, usually at high speeds. However, the said coating methods are non-contoured (with the exception of air-knife coating method) onto rough substrates which means that any irregular substrate surface will lead to non-uniform coating thickness, which may result in irregularities during the printing process.

15 Curtain coating methods are now being developed in the paper industry for coating paper webs, to achieve uniformity in surface application which is a necessary condition for obtaining a good final print rendering.

Curtain coating processes are well known and widely used for the application of one or more liquid layers onto the surface of a moving support in the photographic
20 industry. Indeed, this technology was developed for photographic films that require the deposit of many different coats, usually between 8 and 10, with severe constraints on the surface condition and also the thickness of applied coats.

Curtain coating is a pre-metered coating process which means that only the required amount of coating liquid needed on the web is pumped through the
25 coating head. The curtain coating process is based on free flow on a surface from a coating head located above the surface to be coated. The support is coated by forming a freely-falling vertical curtain of liquid so that it impinges onto the support. A controlled relationship is maintained between the flow rate of the liquid and the speed at which the support is moved so that the curtain is stable and has a
30 uniform flow rate across its width to obtain a layer of the coating onto the substrate. The coating head is defined using properties of the coating fluid, so as to obtain the most uniform possible coating film thickness in the running direction or the transverse direction of the machine.

One of the advantages of curtain coating is the superior quality and more uniform
35 surface of the substrates, namely paper webs, that can be attained.

Another advantage is the lack of contact between the coating head and the support, unlike contact coating processes such as blade and rod coating. This provides a

means of eliminating forces applied on the support during coating, which causes web breakage in particular, and can have a non-negligible effect on the increase in the machine speed, and consequently can reduce production costs.

Another advantage of curtain coating is the possibility of applying two or more coats simultaneously.

Despite many attempts to coat substrate webs with one or more coating layers using curtain coating processes, the main limiting factors to curtain coating remain the curtain stability and the air entrainment, which gives rise to the inclusion of air between the coating composition and the web leading to numerous bubbles and irregularities in the coating. Puddling of the curtain can also be an issue and lead to the formation of a heel at the curtain impingement zone, usually as a result of the coating fluid being too low in viscosity. This phenomenon can lead to coating non-uniformities, and can also induce air entrainment at relatively low web speeds. Highly viscous and elastic curtains tend to ‘pull’ along the web, which can also lead to a non-uniform coating due to fluctuations at the curtain impingement zone.

In curtain coating, uniform layer(s) are only obtained if the operational variables are held within fairly precise limits. These limits define the coating ‘window’. One example is air entrainment, as described in US Patent No. 5,391,401 (Blake et al.). This patent describes a method to alleviate the issues of air entrainment. Therein is described an optimum relationship between viscosity and shear rate for curtain coating. The desired rheological profile promotes a low viscosity at the shear rates expected near the dynamic wetting line, where the coating wets the substrate, and a high viscosity at the much lower shear rates expected in the other regions of the flow. Coating composition can be increased in viscosity by the addition of thickening agents that interact with the binder, which has the effect of increasing the mix viscosity at low shear rate without substantially raising its viscosity at high shear rate, implying that a high viscosity at high shear rate is a disadvantage. Much of this work has been recorded for formulation containing binder, especially gelatine, along with silver halide grains for use in photographic applications. US Patent 5,393,571 (Suga et al.) describes the alleviation of air entrainment and puddling of the curtain coating by using a mix of viscosity superior to 90 mPa.s at low shear rate (10 s^{-1}) onto a rough surface ($0.3\text{ }\mu\text{m}$). US Patent 6,099,913 (Clarke et al.) describes the formation of a coated layer adjacent to the substrate surface having a viscosity of 90 mPa.s to 220 mPa.s at a shear rate of 10000 s^{-1} , which can form a free-falling curtain and allows for higher coating speeds to be attained without air entrainment. These applications are apparently

suitable for photographic formulations generally containing gelatine and silver halide grains, which typically have a low solids content.

5 A second example of a limiting factor is curtain stability which is related to the ratio of inertial to surface tension forces (Weber number). This implies that higher flow rates and lower surface tensions are beneficial to curtain stability. However, in certain cases high flow rates are undesirable especially when high solid content mixes are used and lower coat weights are required.

10 Many typical paper coating compositions are highly pigmented and of high solids content and inherently are shear-thinning (pseudo-plastic) in nature. This type of rheology is useful for applications with blade, bar, reverse roll, slot or slide coating techniques. However, it has been observed that numerous pigmented paper coating formulations do not form a stable curtain at low flow rates (especially when Q, the flow rate per unit die length, is equal to or less than $10^{-4} \text{ m}^3/(\text{s.m})$ for aqueous systems).

15 If the curtain coating method is to be used to coat high solid content paper formulations at low coat weights, this can only be achieved currently by utilising faster web speeds. However, at faster web speeds air entrainment becomes a real issue especially when coating onto smooth, less porous substrates.

20 Diluting the mix in order to run at slower web speeds is not an option. High solids mixes are preferred in the coating process as there is less demand on the drying capacity and it allows for lower grammage raw base ($<80 \text{ g/m}^2$) to be used, which can readily break during the process under high wet coating weights. Higher solid content mixes impart improved properties on the coated media, for example, higher gloss. Diluting mixes also lowers mix viscosity, which can lead to heel formation at the curtain impingement zone, if it becomes too low.

INVENTION

Thus, there is a requirement to generate coating formulations which can generate a stable curtain under low flow rates.

30 Described herein is an improved coating process for pigmented coatings which allows the coating ‘window’, including the curtain stability and coating uniformity, to be expanded. This means that the coating process can be run at a wider range of web speeds, reduced flow rates and, thus, lower corresponding wet lay down and dry coat weight, without destabilising the curtain. A further option
35 allowed is the ability to coat onto smoother, coated substrates, which tend to give rise to the onset of air entrainment more readily than rougher substrates as the web

speed is increased. This offers a greater flexibility with the entire coating process and allows for a greater success in producing high quality coated substrates such as paper, board and plastic webs.

This is achieved by the combined addition of a small quantity of a polymeric additive (rheology modifier) and a non-ionic surfactant to the aqueous coating composition. The former (i.e. rheology modifier) increases the viscosity of the coating composition under mid to high shear rates, and the latter (i.e. non-ionic surfactant) lowers the surface tension of the coating composition. Extensional viscosity was influenced by the choice and quantity of rheology modifier.

The rheology modifier additives include anionic polyacrylamide / acrylate polymers and ionic hydrophobic polyether types. The advantage of these polymeric additives is that they can be added to the formulation in small quantities (<2% dry weight) with no detrimental impact on the product properties (gloss, opacity, colorimetric coordinates L*a*b*, stiffness, smoothness) or on print performance (image quality, optical density, dry time). The surfactants are preferably selected among non-ionic surfactants.

The combination of surfactant and rheology modifier seems to have a significant influence upon extending the curtain coating 'window' of operation. There were no signs that the increase in mid to high shear rate viscosity due to the presence of the rheology modifiers had any influence on the onset of air-entrainment or puddling at the coating impingement zone.

The invention provides a process of producing a free-falling curtain of an aqueous pigmented composition having a high solids content at a flow rate per unit die length values (Q) equal to or inferior to $1 \times 10^{-4} \text{ m}^3/(\text{s.m})$ for coating onto a moving web.

The said composition contains a surfactant (which lowers the surface tension of the composition) and a polymeric rheology modifier.

More particularly, the invention provides a curtain coating process for coating a substrate with a stable curtain and a uniform coating at low flow rates wherein a free-falling curtain of an aqueous composition comprising a high solids content is coated onto a moving substrate at a flow rate per unit die length value (Q) equal to or inferior to $1 \times 10^{-4} \text{ m}^3/(\text{s.m})$, the said high solids content composition comprising a polymeric rheology modifier and a non-ionic surfactant.

The said rheology modifier is selected from the group comprising water phase thickeners and associative thickeners, or a combination of the two.

The said surfactant is selected from the group of alkyl aryl ethoxylates, alkoxylated acetylenics, alkyl acetylenic diols, non-alkoxyated acetylenics, secondary alcohol alkoxylates, and mixtures thereof.

5 The said composition comprises binders and coating pigments. In particular, the binder is selected from a group consisting of copolymers of styrene, in particular styrene-butadienes or styrene-acrylates, styrene-maleic anhydrides, polyvinyl alcohols, polyvinyl pyrrolidones, carboxymethyl celluloses, starches, proteins, polyvinyl acetates, polyurethanes, polyesters, and mixtures thereof.

10 Preferably, the pigments are selected from calcium carbonates, kaolin, talc, titanium dioxide, silica, alumina, boehmite alumina, barium sulphate, zinc oxide, conductive pigments, aluminium silicate, and mixtures thereof.

The said aqueous composition has a high solids content more than or equal to 50% in dry weight, preferably more than 60 %.

15 The concentration of the said rheology modifier in the composition is less than 5% dry weight and preferably less than 1% dry weight, more preferably less than 0.5% dry weight of the total composition dry weight.

The concentration of the said surfactant in the composition is less than 1% dry weight and preferably less than 0.5% dry weight, more preferably less than 0.3% dry weight of the total composition dry weight.

20 Preferably the viscosity of the said aqueous composition is between 50 and 200mPa.s at a shear rate of 1000 s^{-1} , between 25 and 90 mPa.s at a shear rate of 10000 s^{-1} , and between 20 and 75 mPa.s at a shear rate of $100\,000\text{ s}^{-1}$, all sets of data recorded at 25°C .

25 Preferably, the static surface tension of the aqueous composition is less than 45mN/m.

Preferably, the dry coat weight coated onto the substrate is less than or equal to 12 g/m^2 , preferably less than or equal to 10 g/m^2 .

According to the invention, the substrate is either a fibrous substrate such as a paper or a board, or a plastic web.

30 Preferably, the curtain is coated onto a continuous paper web substrate which is either a) non-coated or primed, b) pre-coated or pre-primed, c) pre-coated and subsequently calendered.

In particular, when the substrate is a paper substrate, the grammage of the said paper substrate before coating is less than or equal to 150 g/m^2 , more particularly less than or equal to 80 g/m^2 .

35 The free-falling curtain is comprised of one or more layers.

According to a particular embodiment of the invention, the free-falling curtain is comprised of two layers of aqueous composition with a high solids content as above described.

According to another aspect of the invention there is provided a coated product including a substrate and a substantially uniform coating on the substrate, the coating comprising a high solids content composition including a polymeric rheology modifier and a non-ionic surfactant.

The invention provides a paper or plastic support (web or sheet) obtained from this process, in particular a high gloss paper.

10

EXAMPLES:

Examples of rheology modifiers utilised are outlined in Table 1 and examples of surfactants utilised are outlined in Table 2.

15

Table 1.

Rheology Modifier	Company	Polymer Type	Mode of Activity	Major Feature
Sterocoll BL	BASF	Anionic water-in-oil emulsion of an acrylamide-acrylic acid copolymer	Water phase thickener	Mid-shear rate viscosity-build. Extensional viscosity build
Rheolate 212	Elementis	Hydrophobic ethoxylated polyurethane	Associative thickener	High-shear rate viscosity-build
Rheolate 350	Elementis	Polyether polyol	Associative thickener	High-shear rate viscosity-build
Rheolate 425	Elementis	Hydrophobic modified alkali swellable polyacrylate	Water phase / Associative thickener	Low/mid-shear rate viscosity-build
Rheovis 802	CIBA	Anionic polyacrylamide/acrylate	Water phase thickener	High/mid shear rate viscosity-build
Mowiol 40-88	Kuraray	Polyvinyl alcohol	Water phase thickener	High/mid shear rate viscosity-build. Extensional viscosity build

20

Table 2.

Surfactant	Company	Molecule Type
Surfynol CT211	Air Products	Alkyl acetylenic diol
Surfynol 420	Air Products	Ethoxylated acetylenic
Surfynol 2502	Air Products	Ethoxylated/Propoxylated acetylenic
Surfynol 485	Air Products	Ethoxylated acetylenic
Dynol 604	Air Products	Non-ethoxylated acetylenic
Tergitol 15-S-7	DOW	Secondary alcohol ethoxylate
Tergitol 15-S-9	DOW	Secondary alcohol ethoxylate
Tergitol TMN6	DOW	Branched secondary alcohol ethoxylate
Triton X100	DOW	Octylphenol ethoxylate
Dapro W77	Elementis Specialities	Ethoxylated fatty acid ester

Substrate

150 g/m² clay-coated substrate composing of 130 g/m² raw paper base with 20g/m² clay coating calendered at 10⁵N/m using a 2-nip steel roller calender stack at 600m/min. The physical properties of the coated paper substrate are shown in Table 3.

Table 3.

Parameter	Value
Total Surface Energy (Dyne/cm)	41.4
Contact Angle (°) water	81.7
Contact Angle (°) bromonaphthalene	29.8
Bekk Smoothness (sec)	4135
Bendtsen Air Permeability (mL/min)	0
Gloss (75°) (%)	24.7

10

EXAMPLES**Example 1 (Comparative)**

Calcium carbonate pigments (85 parts) were dispersed in water. A latex binder (15 parts) was added to the formulation and the mix was allowed to stir for 0.5h. The 15 solids content of the formulation was recorded at 64.7%.

Example 2 (Comparative)

Calcium carbonate pigments (84.8 parts) were dispersed in water. A latex binder (14.97 parts) was added to the formulation and the mix was allowed to stir for 0.5h. Surfynol CT211 (0.23 parts) was added to the mix and allowed to stir for a further 0.5h. The solids content of the formulation was recorded at 65.5%.

20

Example 3 (Invention)

Calcium carbonate pigments (84.62 parts) were dispersed in water. A latex binder (14.94 parts) was added to the formulation and the mix was allowed to stir for 0.5h. Surfynol CT211 (Air Products) (0.23 parts) was added to the mix and allowed to stir for a further 0.5h. 0.21 parts of Sterocoll BL (BASF) was added at the end of the formulation. The mix was stirred for a further 0.5h. The solids content of the formulation was recorded at 65.08%.

Example 4 (Invention)

Calcium carbonate pigments (84.44 parts) were dispersed in water. A latex binder (14.90 parts) was added to the formulation and the mix was allowed to stir for 0.5h. Surfynol CT211 (0.23 parts) was added to the mix and allowed to stir for a further 0.5h. 0.42 parts of Rheovis 802 (CIBA) was added at the end of the formulation. The mix was stirred for a further 0.5h. The solids content of the formulation was recorded at 65.0%.

Example 5 (Invention)

Calcium carbonate pigments (84.44 parts) were dispersed in water. A latex binder (14.9 parts) was added to the formulation and the mix was allowed to stir for 0.5h. Surfynol CT211 (0.23 parts) was added to the mix and allowed to stir for a further 0.5h. 0.42 parts of Mowiol 40-88 (Kuraray) was added at the end of the formulation. The mix was stirred for a further 0.5h. The solids content of the formulation was recorded at 63.5%.

Example 6 (Invention)

Calcium carbonate pigments (90.52 parts) were dispersed in water. A latex binder (8.42 parts) was added to the formulation and the mix was stirred. Surfynol CT211 (0.27 parts) was added to the mix. 0.03 parts of a defoamer was added to the mix, followed by the addition of 0.41 parts of Mowiol 4-98 (as a rheology modifier) (Kuraray) and 0.05 parts of Sterocoll BL (BASF), agitation was performed between each component addition. The mix pH was adjusted to 10.3 with sodium hydroxide.

The solids content of the formulation was recorded at 65.5%.

Results and Discussion

Example 1 did not contain either the surfactant or rheology modifier and a curtain could only be formed at a Q (flow rate per unit die length) value of 1.8×10^{-4} m³/(s.m). The static surface tension was measured at 45 mN/m. At a web speed of

5 400 m/min this corresponded to a dry coat weight of 26.6 g/m² which is far greater than the coat weight requirement of <10 g/m² for coated paper of good quality (image quality and dry time) for off-set printing. However, the coating was unstable at the impingement zone, possible due to air entrainment, and a poor coating uniformity was obtained. The viscosity of the mix at a shear rate of 100 s⁻¹
10 was 125mPa.s, at a shear rate of 1000 s⁻¹ was 37mPa.s, at a shear rate of 10 000 s⁻¹ was 14mPa.s, and at a shear rate of 100 000 s⁻¹ was 13mPa.s.

Example 2 involved the addition of the non-ionic surfactant to Example 1 which allowed for the curtain to form at a much reduced flow-rate per unit die length (Q= 9.26×10^{-5} m³/(s.m), in comparison to Example 1. This is due to the lowering of the
15 surface tension of the mix to 35 mN/m. This allows for a dry coat weight of 14.0 g/m² to be attained, which is much lower than in the absence of surfactant but higher than the target 10 g/m². The viscosity of the mix at a shear rate of 100 s⁻¹ was 142mPa.s, at a shear rate of 1000 s⁻¹ was 43mPa.s, at a shear rate of 10 000 s⁻¹ was 18mPa.s, and at a shear rate of 100 000 s⁻¹ was 18mPa.s.

20 Example 3 involved the addition of the surfactant and rheology modifier (Sterocoll BL) to Example 1, which yielded a stable curtain at a flow rate per unit die length, Q, of 6.73×10^{-5} m³/(s.m). This yielded a dry coat weight of 9.4g/m² which was within the target required. The static surface tension is increased over Example 1 (rheology modifiers tend to raise the surface tension), to 40 mN/m. However, the
25 flow rate required for curtain stability is lower than that in Example 1. A uniform coating profile was obtained until a speed of 600 m/min was reached, where the onset of air entrainment occurred. The viscosity of the mix at a shear rate of 100 s⁻¹ was 438mPa.s, at a shear rate of 1000 s⁻¹ was 107mPa.s, at a shear rate of 10 000 s⁻¹ was 50mPa.s, and at a shear rate of 100 000 s⁻¹ was 48mPa.s.

30 Example 4 involved the addition of the surfactant and rheology modifier (Rheovis 802) to Example 1, which yielded a stable curtain at a flow rate per unit die length, Q, of 6.17×10^{-5} m³/(s.m). This yielded a dry coat weight of 8.5g/m² which was within the target required. The static surface tension is increased over Example 1 (rheology modifiers tend to raise the surface tension), to 37 mN/m. However, the
35 flow rate required for curtain stability is again lower than that in Example 1. A uniform coating profile was obtained until a speed of 600m/min was reached,

where the onset of air entrainment occurred. The viscosity of the mix at a shear rate of 100s^{-1} was 355mPa.s, at a shear rate of 1000s^{-1} was 80mPa.s, at a shear rate of $10\,000\text{s}^{-1}$ was 28 mPa.s, and at a shear rate of $100\,000\text{s}^{-1}$ was 24 mPa.s.

Example 5 involved the addition of the surfactant and Mowiol 40-88 polyvinyl alcohol to Example 1, which yielded a stable curtain at a flow rate per unit die length, Q, of $7.86 \times 10^{-5}\text{ m}^3/(\text{s.m})$. This yielded a dry coat weight of 10.0 g/m^2 which was within the target required. The static surface tension is increased over Example 1 to 42 mN/m. However, the flow rate required for curtain stability is lower than in Example 1. A uniform coating profile was obtained until a speed of 600 m/min was reached, where the onset of air entrainment occurred. The viscosity of the mix at a shear rate of 100s^{-1} was 161mPa.s, at a shear rate of 1000s^{-1} was 124mPa.s, at a shear rate of $10\,000\text{s}^{-1}$ was 77mPa.s, and at a shear rate of $100\,000\text{s}^{-1}$ was 34mPa.s.

Example 6 involved the addition of the surfactant and a dual rheology modifier system (Sterocoll BL + Mowiol 4-98) to a latex binder and calcium carbonate coating mix. A stable curtain at a flow rate per unit die length Q of $9.45 \times 10^{-5}\text{ m}^3/(\text{s.m})$ was formed and the static surface tension value was of 35.5 mN/m. A uniform coating profile was obtained without air entrainment at a line speed of 600m/min. The coated paper obtained presents good print performance. The dry coat weight was of 10.0g/m^2 . The viscosity of the mix at a shear rate of 100s^{-1} was 255 mPa.s, at a shear rate of 1000s^{-1} was 78mPa.s, at a shear rate of $10\,000\text{s}^{-1}$ was 37mPa.s, and at a shear rate of $100\,000\text{s}^{-1}$ was 29mPa.s.

Viscosity results at the various shear rates for each mix are summarised in Table 4.

Table 4

Example No.	Surfactant Present	Rheology Modifier/ % dry parts	Shear Rate (s^{-1})				
			10	100	1 000	10 000	100 000
1	none	none	442	125	37	14	13
2	yes	none	544	142	43	18	18
3	yes	0.21% Sterocoll BL	2411	438	107	50	48
4	yes	0.42% Rheovis 802	1914	355	80	28	24
5	yes	0.42% Mowiol 40-88	2252	427	94	37	34
6	yes	0.05% Sterocoll BL 0.41% Mowiol 4-98	1350	255	78	37	29

Effective extensional viscosity does not appear to impact on curtain stability (see the results in Table 5). Example 3 shows a high extensional viscosity of 174mPa.s

at 100 000 s⁻¹ and Example 4 shows a low extensional viscosity of 4mPa.s at the same shear rate, yet the minimum flow rate obtained for curtain stability is slightly lower for the latter.

5

Table 5

Example No.	Effective Extensional Viscosity (mPa.s) at shear rate of 100 000 s ⁻¹
1	0
2	0
3	174
4	4
5	1
6	150

Table 6

Example No.	Qmin (curtain self-forms) (m ³ /(s.m))	Web Speed (m/min)	Mix Solids (%)	Dry Coat Weight (g/m ²)	Mix Density (g/cm ³)	Mix Static Surface Tension (mN/m)	Air Entrainment
1	1.80x10 ⁻⁴	400	64.7	26.6	1.526	47	Yes (≥200m/min)
2	9.26x10 ⁻⁵	400	65.5	14.0	1.538	35	No
3	6.73x10 ⁻⁵	400	65.1	9.4	1.423	40	No
4	6.17x10 ⁻⁵	400	65.0	8.5	1.410	37	No
5	7.74x10 ⁻⁵	400	63.5	10.0	1.354	42	No
6	9.45x10 ⁻⁵	600	65.5	10.0	1.61	35.5	No

10

Test Methods

Viscosity – was measured using a Brookfield RVT viscometer. The spindle speed selected was 100rpm. Spindle size was either sp2 or sp3. The temperature of the mix was recorded during the measurement of viscosity.

Density – was measured using a 100mL Pycnometer. The temperature was recorded during the measurement of the density.

pH – was measured using an HI 9024 Microcomputer pH meter (Hanna Instruments). The temperature was recorded during the measurement of the pH.

20 Solids (%) – was measured using a CEM Labwave 9000 Microwave Moisture/Solids Analyzer.

Contact Angle – was measured with a FibroDAT 1100.

Surface Tension – was measured using a DCA 132 apparatus with a platinum plate.

5 *Paper Gloss* – was measured using a gloss meter at a fixed angle of 75° (BYK Gardner GmbH).

Paper Smoothness – was measured using a Bekk Smoothness Tester (Messmer Instruments Ltd).

Air Permeability – was measured using a Bendtsen Tester (Lorentzen & Wettre)

10 *Rheology* – flow data was measured with a CV0120 High Resolution Rheometer (Bohlin Instruments) using the parallel plate at a gap of 40 µm at 25 +/- 0.1 °C. The shear rate range was 10 to 100 000 s⁻¹.

15 *Effective Extensional viscosity* - was measured on a Paar Automated High Shear Viscometer HVA 6 with a capillary length of 10mm and 5 mm and a capillary diameter of 0.6 mm.

Mix Preparation and Coating Method

All parts are expressed in dry weight by 100 parts in dry weight of the total composition.

20 So, the coating formulas in examples 1-6 are expressed in % dry weight (parts) of the total composition.

All formulations were mixed using a Greaves GM dispersing apparatus. The stirring was optimised to ensure good mixing but to avoid excessive air entrainment. The curtain head used was a slide-type with a width of 0.49m and a die gap of 300µm. The curtain coating head was equipped with edge guides with 25 running water down each side, with a vacuum suction present to remove this water at the bottom of the edge guides. The catch pan also acts as a baffle – a mechanical barrier to limit air entrainment at the impingement zone. A suction vacuum can optionally be applied (0.3 bar) to reduce the movement across the web of the curtain at the impact zone and to limit further the onset of air entrainment.

30 The curtain height was 100mm.

The coat weight of each coated sample is determined from the known volumetric flow rate of the pump delivering the mix to the curtain head, web speed, density and % solids of the mix, and curtain width. The coat weight is 35 checked by placing a 100 cm² coated and uncoated substrate sample in an oven at

150°C for 10 min and measuring the difference in weight between the two samples.

Materials used in Formulations

- 5 Calcium carbonate pigments : ground calcium carbonate of which 95% (weight) have an average particle size less than 2.5 µm. Solids at 78%.
- 10 Latex binder : an aqueous dispersion of a copolymer of styrene–butadiene. Solids content are at 50%.
- 10 Mowiol 40-88 (Kuraray): the polyvinyl alcohol is 88% hydrolysed. The viscosity of a 4% solution at 25°C is 40 cps as measured on a Brookfield RVT viscometer (manufacturer's data). Used as a rheology modifier (water phase thickener) or as a binder. The polyvinyl alcohol was used as a 10% solution obtained by heating the polyvinyl alcohol granules with water at 95°C for 0.5h.
- 15 Rheovis 802: an anionic water-in-oil emulsion of a polyacrylamide/acrylate. Used as a rheology modifier (water phase thickener).
- 15 Mowiol 4-98 (Kuraray): the polyvinyl alcohol is 98% hydrolysed. The viscosity of a 4% solution at 25°C is 4.5 cps as measured on a Brookfield RVT viscometer (manufacturer's data). Used as a rheology modifier (thickener) or as a binder. The Mowiol 4-98 was used as a 25% solution obtained by heating the polyvinyl alcohol granules with water at 95°C for 0.5h.

CLAIMS

1. Curtain coating process for coating substrates with a stable curtain and a uniform coating at low flow rates wherein a free-falling curtain of an aqueous composition comprising a high solids content is coated onto the moving substrate at a flow rate per unit die length value (Q) equal to or inferior to $10^{-4} \text{ m}^3/(\text{s.m})$, the said high solids content composition comprising a polymeric rheology modifier and a non-ionic surfactant.
2. Curtain coating process as claimed in claim 1, wherein the said rheology modifier is selected from the group comprising water phase thickeners and associative thickeners, and mixtures thereof.
3. Curtain coating process as claimed in claim 2, wherein the said water phase thickeners are selected among anionic polyacrylamide/acrylate polymers, ionic hydrophobic polyether types and Polyvinyl alcohol, carboxymethyl cellulose, hydroxyethyl cellulose, starch, protein derivate and alkali swellable polyacrylate(s).
4. Curtain coating process as claimed in claim 2, wherein the said associative thickeners are selected among hydrophobic ethoxylated polyurethanes and polyether polyols.
5. Curtain coating process as claimed in claims 1 to 4, wherein the said surfactant is selected from the group of alkyl aryl ethoxylates, alkoxyolated acetylenics, alkyl acetylenic diols, non-alkoxyolated acetylenics, secondary alcohol alkoxylates, and mixtures thereof.
6. Curtain coating process as claimed in any one of claims 1 to 5, wherein the aqueous composition has a high solids content more than or equal to 50% dry weight, preferably more than or equal to 60%.
7. Curtain coating process as claimed in any one of claims 1 to 6, wherein the viscosity of the aqueous composition is between 50 and 200mPa.s at a shear rate of 1000 s^{-1} , between 25 and 90mPa.s at a shear rate of $10\ 000 \text{ s}^{-1}$, and between 20 and 75 mPa.s at a shear rate of $100\ 000 \text{ s}^{-1}$, all sets of data recorded at 25°C.

8. Curtain coating process as claimed in any one of claims 1 to 6, wherein the static surface tension of the aqueous composition is less than 45 mN/m.
9. Curtain coating process as claimed in any one of claims 1 to 8, wherein the aqueous composition comprises binders and pigments.
10. Curtain coating process as claimed in claim 9, wherein the binder is selected from a group consisting of copolymers of styrene in particular styrene-butadiene or styrene-acrylates, styrene-maleic anhydrides, polyvinyl alcohols, polyvinyl pyrrolidones, carboxymethyl celluloses, starch, protein, polyvinyl acetates, polyurethanes, polyester, acrylic acid and mixtures thereof.
11. Curtain coating process as claimed in claim 9 or claim 10, wherein the pigment is selected from calcium carbonates, aluminium silicate, kaolin, talc, titanium dioxide, silica, aluminas, boehmite alumina, barium sulphate, zinc oxide, plastic pigments, conductive pigments, and mixtures thereof.
12. Curtain coating process as claimed in any one of claims 1 to 9, wherein the concentration of rheology modifier in the aqueous composition is less than 5% dry weight and preferably less than 1% dry weight of the total composition dry weight.
13. Curtain coating process as claimed in any one of claims 1 to 10, wherein the concentration of surfactant in the composition is less than 1% dry weight and preferably less than 0.5% dry weight of the total composition dry weight.
14. Curtain coating process as claimed in any one of claims 1 to 13, wherein the dry coat weight coated onto the substrate is less than or equal to 12g/m², preferably less than or equal to 10 g/m².
15. Curtain coating process as claimed in any one of claims 1 to 14, wherein the moving substrate is a fibrous substrate or a plastic substrate.
16. Curtain coating process as claimed in claim 15, wherein the fibrous substrate is a paper or a board.

17. Curtain coating process as claimed in claim 16, wherein the grammage of the paper substrate before coating is less than or equal to 150g/m², more particularly less than or equal to 80 g/m².
18. Curtain coating process as claimed in claims 16 to 17, wherein the curtain is coated onto a continuous paper web which is either a) non-coated or primed, b) pre-coated or pre-primed, c) pre-coated and subsequently calendered.
19. Curtain coating process as claimed in claim 15, wherein the moving substrate is a plastic web or a film.
20. Curtain coating process as claimed in any one of claims 1 to 19, wherein the free-falling curtain is comprised of one or more layers.
21. Curtain coating process as claimed in claim 20, wherein said free-falling curtain comprises two layers of aqueous composition with a high solids content.
22. A coated product including a substrate and a substantially uniform coating on the substrate, the coating comprising a high solids content composition including a polymeric rheology modifier and a non-ionic surfactant.
23. A coated product as claimed in claim 22, wherein the said rheology modifier is selected from the group comprising water phase thickeners and associative thickeners, and mixtures thereof.
24. A coated product as claimed in claim 22 or claim 23, wherein the said surfactant is selected from the group of alkyl aryl ethoxylates, alkoxyolated acetylenics, alkyl acetylenic diols, non-alkoxyolated acetylenics, secondary alcohol alkoxylates, and mixtures thereof.
25. A coated product as claimed in any one of claims 22 to 24, wherein the coating composition including binders and pigments.
26. A coated product as claimed in any one of claims 22 to 25, wherein the concentration of rheology modifier in the coating composition is less than 5% dry weight and preferably less than 1% dry weight of the total composition dry weight.

27. A coated product as claimed in any one of claims 22 to 26, wherein the dry coat weight coated onto the substrate is less than or equal to 12g/m², preferably less than or equal to 10 g/m².
28. A coated product as claimed in any one of claims 22 to 27, wherein the substrate is a fibrous substrate or a plastic substrate.
29. A coated product as claimed in claim 28, wherein the substrate is a paper substrate having a grammage, excluding the coating, of less than or equal to 150g/m², more particularly less than or equal to 80 g/m².

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TITLE: Curtain coating process for coating substrate involves coating free-falling curtain of high solid containing composition of rheology modifier and non-ionic surfactant onto moving substrate at specific flow rate per unit die length value

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PATENT-ASSIGNEE: ARJO WIGGINS FINE PAPERS LTD[ARJO]

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CN 1989298 A	June 27, 2007	ZH
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DESIGNATED-STATES: AE AG AL AM AT AU AZ BA BB BG BR BW BY BZ CA CH CN CO CR CU CZ DE DK DM DZ EC EE EG ES FI GB GD GE GH GM HR HU ID IL IN IS JP KE KG KM KP KR KZ LC LK LR LS LT LU LV MA MD MG MK MN MW MX MZ NA NG NI NO NZ OM PG P H PL PT RO RU SC SD SE SG SK SL SM SY TJ TM TN TR TT TZ UA UG US UZ VC VN YU ZA ZM ZW AT BE BG BW CH CY CZ DE DK EA EE ES FI FR GB

GH GM GR HU IE IS IT KE LS LT LU LV
 MC MW MZ NA NL OA PL PT RO SD SE
 SI SK SL SZ TR TZ UG ZM ZW AT BE BG
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BR 200513934A	N/A	2005BR- 013934	July 27, 2005
CN 1989298A	N/A	2005CN- 80025426	July 27, 2005
EP 1771624A2	N/A	2005EP-768964	July 27, 2005
EP 1771624A2	N/A	2005WO- GB002947	July 27, 2005
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CIPS	B05D1/30 20060101
CIPS	D21H19/44 20060101
CIPS	D21H19/44 20060101
CIPS	D21H19/44 20060101
CIPS	D21H23/48 20060101

ABSTRACTED-PUB-NO: WO 2006010927 A2**BASIC-ABSTRACT:**

NOVELTY - Curtain coating involves coating a free-falling curtain of an aqueous composition comprising a high solid content onto a moving substrate at a flow rate per unit die length value (Q) less than or equal to 10-4/(s.m.). The high solid content composition comprises a polymeric rheology modifier and a non-ionic surfactant.

USE - For coating substrates (claimed).

ADVANTAGE - The process provides the coated substrate with stable curtain and uniform coating. The process can be run at a wide range of web speed, reduced flow rate, and thus, lower corresponding wet lay down and dry coat weight without destabilizing the curtain. A smooth coated substrate can be further coated to give rise onset of air entrainment more readily than rougher substrates; this offers flexibility with the entire coating process and produces high quality coated substrates.

EQUIVALENT-ABSTRACTS:**INORGANIC CHEMISTRY**

Preferred Components: The pigment is calcium carbonate, aluminum silicate, kaolin, talc, titanium dioxide, silica, alumina, boehmite alumina, barium sulfate, zinc oxide, plastic pigment and/or conductive pigment.

POLYMERS

Preferred Components: The rheology modifier (less than 5, preferably less than 1 wt.%) is water phase thickener and/or associative thickener. The water phase thickener is selected from anionic polyacrylamide/acrylate polymers, ionic hydrophobic polyether types and polyvinyl alcohol, carboxymethyl cellulose, hydroxyethyl cellulose, starch, protein derivate and alkali swellable polyacrylate(s). The associative thickener is selected from hydrophobic ethoxylated polyurethanes and polyether polyols. The surfactant (less than 1, preferably less than 0.5 wt.%) is selected from alkyl aryl ethoxylates, alkoxylated acetylenics, alkyl acetylenic diols, non-alkoxylation acetylenics and/or secondary alcohol.

Preferred Composition: The aqueous composition has a high solids content greater than or equal to 50 (preferably greater than or equal to 60) wt.%. The viscosity of the aqueous composition is 50 - 200 mPa.s at a shear rate of 1000 s-1, 25 - 90 mPa.s at a shear rate of 10000 s-1 and 20 - 75 mPa.s at a shear rate of 100000 s-1 at 25degreesC. The static surface tension of the aqueous composition is less than 45 mN/m. The aqueous composition comprises binders and pigments. The binder is copolymer of styrene (preferably styrene-butadiene or styrene-acrylate), styrene-maleic anhydride, polyvinyl alcohol, polyvinyl pyrrolidone, carboxymethyl celluloses, starch, protein, polyvinyl acetate, polyurethane, polyester and/or acrylic acid.

Preferred Process: The moving substrate is a fibrous substrate (e.g. paper or board) or a plastic substrate (preferably plastic web or film). The grammage of the paper substrate before coating is less than or equal to 150 (preferably less than or equal to 80) g/m². The curtain is coated onto a continuous paper web which is non-coated or primed, pre-coated or pre-primed or pre-coated and subsequently calendered. The free-falling curtain is comprised of at least one layer (preferably two layers of the aqueous composition). The Process provides dry coating (less than or equal to 12, preferably less than or equal to 10 g/m²) on the substrate.

Calcium carbonate pigments (90.52 parts) were dispersed in water. A latex binder (8.42 parts) was added to it and stirred. Surfynol CT211 (RTM; ethoxylated acetylenic compound) (0.27 parts), defoamer (0.03 parts), and Mowiol 4-98 (RTM; rheology modifier) (0.41 parts), Sterocoll BL (RTM; acrylamide-acrylic acid copolymer) (0.05 parts) were added to the mixture. Sodium hydroxide was added to the mixture to adjust pH at 10.3. The solids

content of the formulation was 65.5%. Viscosity of the formulation at a shear rate of 100 s⁻¹ was 255 mPa.s. A stable curtain at a flow rate per unit die length (Q) of 9.45x10⁻⁵ m³/(s.m.) was formed and the static surface tension value was 35.5 mN/m.

TITLE-TERMS: CURTAIN COATING PROCESS SUBSTRATE FREE FALL HIGH SOLID CONTAIN COMPOSITION RHEOLOGICAL MODIFIED NON ION SURFACTANT MOVE SPECIFIC FLOW RATE PER UNIT DIE LENGTH VALUE

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Polymer Index [1.5] 2004 ; G3678 G3634 D01 D03 D11 D10 D23 D22 D31 D42 D50 D60 D76 D92 F24 F34 F38 F35 H0293 P0599 G3623 R01835 133912;

Polymer Index [1.6] 2004 ;
G0635 G0022 D01 D12 D10
D23 D22 D31 D41 D51 D53
D58 D75 D86 F71; G0566
G0022 D01 D11 D10 D12 D51
D53 D58 D63 D84 F41 F89
R00835 829; G0282 G0271
G0260 G0022 D01 D12 D10
D26 D51 D53 D58 D60 D83
F36 F35 R00446 1911; H0000;
P0088; P0099;

Polymer Index [1.7] 2004 ;
P1694*R D01;

Polymer Index [1.8] 2004 ;
H0022 H0011; G0102 G0022
D01 D02 D12 D10 D19 D18
D31 D51 D53 D58 D76 D88
R00708 368; G0340*R G0339
G0260 G0022 D01 D12 D10
D26 D51 D53 D58 D63 F41
F89; P1741; P0088;

Polymer Index [1.9] 2004 ;
H0022 H0011; G0102 G0022
D01 D02 D12 D10 D19 D18
D31 D51 D53 D58 D76 D88
R00708 368; G0828 G0817
D01 D02 D12 D10 D51 D54
D56 D58 D84 R00806 129411;
P0328; P1741; P0351;

Polymer Index [1.10] 2004 ;
H0022 H0011; G0102 G0022
D01 D02 D12 D10 D19 D18

D31 D51 D53 D58 D76 D88
R00708 368; G0760 G0022
D01 D23 D22 D31 D42 D51
D53 D59 D65 D75 D84 F39
E00 E01 R00843 790; P1741;

Polymer Index [1.11] 2004 ;
ND04; K9483*R; K9563
K9483; Q9999 Q7114*R;
B9999 B3554*R; B9999
B5390 B5276; Q9999 Q6791;
ND07; K9574 K9483;
K9676*R; N9999 N7147
N7034 N7023; N9999 N6940
N6939;

Polymer Index [1.12] 2004 ;
G3190 D00 F80 O* 6A Mg 2A
Si 4A R01541 108296 147554;
D00 F44 C* 4A O* 6A Ca 2A
R01278 89827; D00 F80 O*
6A Al 3A Si 4A R01949
129788; D00 F20 Ti 4B Tr O*
6A R01966 686; D00 F20 O*
6A Si 4A R01694 107016; D00
F20 Al 3A O* 6A R01544 92;
D00 F60 O* 6A S* Ba 2A
R01739 88364; D00 F20 Zn 2B
Tr O* 6A R01520 866; A999
A102 A077; A999 A771;

Polymer Index [1.13] 2004 ;
A999 A691*R; A999 A715
A691; A999 A771;

Polymer Index [1.14] 2004 ;
D01 D11 D10 D18*R F34;

D01 D11 D10 D12*R D52 D51
F34; A999 A566*R; K9325;
A999 A771;

Polymer Index [2.1] 2004 ;
P0000; S9999 S1285*R;

Polymer Index [2.2] 2004 ;
N9999 N7090 N7034 N7023;
B9999 B5447 B5414 B5403
B5276; ND07; K9574 K9483;
K9676*R; N9999 N7147
N7034 N7023; N9999 N6940
N6939;

Polymer Index [3.1] 2004 ;
A999 A691*R; A999 A715
A691; A999 A782; P1036
P0964 F34 D01;

Polymer Index [3.2] 2004 ;
G1558 D01 D23 D22 D31 D42
D50 D73 D82 F47 R00351
444; A999 A691*R; A999
A715 A691; A999 A782;
H0011*R; P0055; P1058*R
P1592 P0964 H0260 F34 F77
H0044 H0011 D01;

Polymer Index [3.3] 2004 ;
G0340*R G0339 G0260 G0022
D01 D12 D10 D26 D51 D53
D58 D63 F41 F89; A999
A691*R; A999 A715 A691;
A999 A782; H0000; H0011*R;
P0088;

Polymer Index [3.4] 2004 ;
G3714*R P0599 D01 F70;
A999 A691*R; A999 A715
A691; A999 A782; M9999
M2391;

Polymer Index [3.5] 2004 ; D01
D11 D10 D23 D22 D31 D42
D50 D76 D86 F24 F29 F26
F34 H0293 P0599 G3623
R01863 107779; A999
A691*R; A999 A715 A691;
A999 A782;

Polymer Index [3.6] 2004 ;
G3678 G3634 D01 D03 D11
D10 D23 D22 D31 D42 D50
D76 D92 F24 F29 F26 F34
H0293 P0599 G3623 R01859
133920 97261; A999 A691*R;
A999 A715 A691; A999 A782;

Polymer Index [3.7] 2004 ;
G3678 G3634 D01 D03 D11
D10 D23 D22 D31 D42 D50
D60 D76 D92 F24 F34 F38
F35 H0293 P0599 G3623
R01835 133912; A999
A691*R; A999 A715 A691;
A999 A782;

Polymer Index [3.8] 2004 ;
A999 A691*R; A999 A715
A691; A999 A782; P1707
P1694 D01;

Polymer Index [3.9] 2004 ;

A999 A691*R; A999 A715
A691; A999 A782; P0964*R
F34 D01;

Polymer Index [3.10] 2004 ;
G0340*R G0339 G0260 G0022
D01 D12 D10 D26 D51 D53
D58 D63 F41 F89; G0453
G0260 G0022 D01 D12 D10
D26 D51 D53 D58 D83 F70
F93 R00444 8781; A999
A691*R; A999 A715 A691;
A999 A782; H0022 H0011;
P0964*R F34 D01; K9621*R;
P0088;

Polymer Index [3.11] 2004 ;
B9999 B3509 B3485 B3372;

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